

Please amend the paragraph starting with "Further, when the amount of water..."
on page 20, line 4 to read as follows:

AG --Further, when the amount of water vapor contained in a reformed gas is from 24 to 50% by volume, particularly high activity is obtained. It is more preferable from the equilibrium point of view when the average content of water vapor in the reformed gas is higher, and specifically, the CO concentration fully decreases when water vapor is contained in an amount of 24% by volume or more. On the other hand, when the water vapor content increases, the flow rate increases causing a disadvantage in the reaction rate, and specifically, when the content is more than 50% by volume, the CO concentration cannot be decreased sufficiently.—

In the claims:

Please amend claims 1 and 6-7, without prejudice, to read as follows, with the changes shown in the attached Marked-Up Version of the Claims in which additions are shown by underlining and deletions are shown in brackets:

AG - 1 (Amended) A hydrogen refinement apparatus comprising a source of reformed gas containing at least a hydrogen gas, carbon monoxide and water vapor, and a reaction chamber equipped with a carbon monoxide shifting catalyst body positioned downstream from said reformed gas source,

wherein said carbon monoxide shifting catalyst body comprises a carrier composed of at least one metal oxide having a BET specific surface area of at least 10 m²/g and Pt supported thereon, such that carbon monoxide in said reformed gas is capable of being reduced by a shift reaction in said reaction chamber.

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6. (Amended) A hydrogen refinement apparatus in accordance with claim 1, wherein said carbon monoxide shifting catalyst body comprises a carrier supporting Pd, Rh or Ru in an amount of 0.1 to 0.5 fold by weight based on Pt, in addition to Pt.

7. (Amended) A method for operating a hydrogen refinement apparatus comprising a source of reformed gas containing at least a hydrogen gas, carbon monoxide, and water vapor and a reaction chamber equipped with a carbon monoxide shifting catalyst body positioned downstream from said reformed gas source; said carbon monoxide shifting catalyst body comprising a carrier composed of at least one metal oxide having a BET specific surface area of at least 10 m²/g and Pt supported thereon, comprising the steps of controlling the temperature of said carbon monoxide shifting catalyst body from 150 to 450 °C and reducing carbon monoxide in said reformed gas by a shift reaction in said reaction chamber. - -

Please add new claims 10-15 to read as follows:

- 10. (New) The hydrogen refinement apparatus of claim 1, wherein the carrier is in a form of pellets.

11. (New) The hydrogen refinement apparatus of claim 10, wherein the pellets are located inside a column.

12. (New) The hydrogen refinement apparatus of claim 1, wherein a surface of the carrier is composed of a slurry coating of a heat-resistant metal material.

13. (New) The hydrogen refinement apparatus of claim 12, wherein the metal material is selected from the group consisting of cordierite and mullite.

14. (New) The hydrogen refinement apparatus of claim 1, wherein the carrier is in a form of a honeycomb.